We claim:

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- 1. A method of treating tertiary butyl alcohol containing a minor amount of impurities which comprises contacting the tertiary butyl alcohol in the liquid phase with aluminum oxide and a large pore zeolite, and recovering a tertiary butyl alcohol product stream reduced in content of the impurities.
- **2.** The method of claim **1** wherein the large pore zeolite has an average pore size from about 6 Angstroms to about 15 Angstroms
 - 3. The method of claim 1 wherein the large pore zeolite is zeolite X.
 - **4.** The method of claim 1 wherein the large pore zeolite is zeolite Y.
- 5. The method of claim 1 wherein the large pore zeolite is in the sodium form.
- 6. The method of claim 1 wherein the aluminum oxide is selected from the group consisting of α -alumina, γ -alumina, activated alumina, and basic alumina.
- 7. The method of claim 6 wherein the aluminum oxide is activated alumina.
- 8. The method of claim 1 wherein the aluminum oxide has a surface area in the range of from about 50 to about 500 m^2/g .
- **9.** The method of claim **1** wherein the tertiary butyl alcohol is contacted with an additional adsorbent comprising a molecular sieve having an average pore size of about 3 to about 5 Angstroms.
- **10.** The method of claim **9** wherein the molecular sieve is selected from the group consisting of 3A, 4A, and 5A.
 - 11. The method of claim 9 wherein the molecular sieve is 4A.
- 12. A method of treating tertiary butyl alcohol containing impurities which comprises contacting the tertiary butyl alcohol with activated alumina, a large pore zeolite selected from the group consisting of zeolite Y and zeolite X, and a molecular sieve selected from the group consisting of 3A, 4A, and 5A, and recovering a tertiary butyl alcohol product stream reduced in content of the impurities.
 - 13. The method of claim 12 wherein the large pore zeolite is in the sodium form.
 - 14. The method of claim 12 wherein the molecular sieve is 4A.